## WE CLAIM:

- 1. A process for the removal of carbon dioxide from flue gas comprising the steps of:
- (a) contacting the flue gas with a solvent in a solvent extraction zone thereby extracting carbon dioxide from flue gas and providing a carbon dioxide-depleted flue gas and a carbon dioxide-containing solvent:
- (b) heating said carbon dioxide-containing solvent to a solvent regeneration temperature and maintaining the solvent at said temperature in a solvent regeneration zone thereby regenerating the solvent and providing a regenerated solvent and a carbon dioxide stream; and
- (c) contacting said carbon dioxide stream with silicate particles dispersed in an aqueous solution in a mineral carbonation zone said silicate particles being a bivalent alkaline earth metal silicate.
- 2. The process of claim 1 wherein the heat released in step (c) is used in step (b).
- 3. The process of claim 1 wherein at least 50% of the heat needed for step (b) is supplied by the heat released in step (c).
- 4. The process of claim 1 wherein the temperature of contact in the mineral carbonation zone is in the range of 25°C to 35°C higher than the solvent regeneration temperature.
- 5. The process of claim 1 wherein the solvent regeneration temperature is in the range of from 100°C and 200°C.
- 6. The process of claim 1 wherein the solvent regeneration temperature is in the range of from 120°C and 180°C.
- 7. The process of claim 1 wherein the carbon dioxide stream obtained in step (b) is pressurized to a

pressure in the range of from 3 to 15 bar (absolute), before being reacted with the silicate in the mineral carbonation zone.

- 8. The process of claim 1 wherein the contact temperature in the mineral carbonation zone is in the range of from 140 to 200 °C.
- 9. The process of claim 1 wherein the solvent is an aqueous amine solution.
- 10. The process of claim 2 wherein the solvent is an aqueous amine solution.
- 11. The process of claim 4 wherein the solvent is an aqueous amine solution.
- 12. The process of claim 9 wherein the solvent is selected from the group consisting of an aqueous solution of monoethanolamine, diethanolamine, triethanolamine, diglycolamine, methyldiethanolamine, disopropanolamine, and a combination of two or more thereof.
- 13. The process of claim 10 wherein the temperature of contact in the mineral carbonation zone is in the range of 25°C to 35°C higher than the solvent regeneration temperature.
- 14. The process of claim 10 wherein the solvent regeneration temperature is in the range of from 100°C and 200°C.
- 15. The process of claim 14 wherein the solvent is selected from the group consisting of an aqueous solution of monoethanolamine, diethanolamine, triethanolamine, diglycolamine, methyldiethanolamine, disopropanolamine, and a combination of two or more thereof.
- 16. The process of claim 1 wherein the bivalent alkaline earth metal silicate is a magnesium or calcium silicate.
- 17. The process of claim 1 wherein the silicates particles have an average diameter of at most 0.5 mm.

- 18. The process of claim 11 wherein the silicates particles have an average diameter of at most 0.2 mm.
- 19. A process for the removal of carbon dioxide from flue gas comprising the steps of:
- (a) contacting the flue gas with a solvent effective to extract carbon dioxide from flue gas in a solvent extraction zone thereby extracting carbon dioxide from flue gas and providing a carbon dioxide-depleted flue gas and a carbon dioxide-containing solvent;
- (b) heating said carbon dioxide-containing solvent to a temperature in the range of from 100°C and 200°C and maintaining the solvent at said temperature in a solvent regeneration zone wherein at least 50% of the heat needed is supplied by the heat released in step
- (c) thereby regenerating the solvent and providing a regenerated solvent and a carbon dioxide stream; and
- (c) contacting said carbon dioxide stream with silicate particles dispersed in an aqueous solution in a mineral carbonation zone said silicate particles being a bivalent alkaline earth metal silicate.
- 20. The process of claim 19 wherein the solvent is an aqueous amine solution.